



KENYATTA UNIVERSITY
EXAMINATION FOR THE DEGREE OF MASTER OF SCIENCE IN RENEWABLE
ENERGY TECHNOLOGY

SET 811: ENERGETICS AND POWER GENERATION SYSTEMS

1ST SEMESTER 2022/2023

TIME: 3 HOURS

INSTRUCTIONS:

- (i) This paper contains **FIVE** questions
- (ii) Attempt any **THREE** questions
- (iii) All questions carry equal marks
- (iv) Steam Tables and Charts are provided

QUESTION 1 (25 MARKS)

- (a) (i) Outline thermodynamic cycles used in power plant analysis (**3 Marks**)
(ii) Discuss FIVE classification methods of steam turbines (**5 Marks**)
- (b) Steam at a pressure of 50 bar and 500°C is supplied to a steam turbine. It comes out at 0.05 bar and 0.85 dry. One stage reheating is used and reheating is carried out up to its original temperature.
 - (i) Determine the theoretical thermal efficiency of the plant.
 - (ii) Find also the pressure at which reheating is carried out. Assume expansions at both stages are isentropic. Show the processes on T-S chart.
 - (iii) If the net work output is 1200 kJ/kg of steam find out the actual efficiency of the plant. (**9 Marks**)
- (c) A pass-out two stage turbine receives steam at 50 bar and 350°C. At 1.5 bar the high pressure stage exhausts and 12000 kg of steam per hour are taken out at this stage for process purposes. The remainder is reheated at 1.5 bar to 250°C and then expanded through the low pressure turbine to a condenser pressure of 0.05 bar. The power output from the turbine unit is to be 3750 kW. Using steam tables or h-s charts, calculate the boiler capacity.

Take isentropic efficiency of the high pressure stage as 0.84 and that of low pressure stage as 0.81. Sketch T-S diagram for the process. (**8 Marks**)

QUESTION 2 (25 MARKS)

(a) Explain the following using illustrations:

- (i) The difference between an open and closed gas turbine (4 Marks)
- (ii) Three modifications on the basic gas turbine cycle using schematic and T-S diagrams (9 Marks)

(b) At the design speed the following data apply to a gas turbine set employing the heat exchanger: Isentropic efficiency of compressor = 75%, isentropic efficiency of the turbine = 85%, mechanical transmission efficiency = 99%, combustion efficiency = 98%, mass flow = 22.7 kg/s, pressure ratio = 6:1, heat exchanger effectiveness = 75%, maximum cycle temperature = 1000 K. The ambient air temperature and pressure are 15°C and 1.013 bar respectively. Calculate:

- (i) The net power output
- (ii) Specific fuel consumption
- (iii) Thermal efficiency of the cycle. Take the calorific value of fuel as 43125 kJ/kg and assume no pressure-loss in heat exchanger and combustion chamber. (14 Marks)

QUESTION 3 (25 MARKS)

(a) Define the following terms as used in power plant engineering:

- (i) Load factor
- (ii) Use factor
- (iii) Capacity factor (3 Marks)

(b) A power station has two 60MW units each running for 1000 hours a year. The energy produced per year is 500×10^6 kW-hr. Calculate the plant load factor and plant use factor. (5 Marks)

(c) What is meant by uranium enrichment? Describe some methods of Uranium enrichment. Compare the economic (cost) of nuclear power plant with steam power plant (7 Marks)

(d) A Nuclear power plant reactor produces electrical power of 400MW. How much ^{235}U is burnt per day, if the plant efficiency is 30%. Assume that 200MeV of energy is released per fission. ($1\text{MeV} = 1.6 \times 10^{-13}\text{J}$) (5 Marks)

- (e) Using schematic diagrams, describe the operational differences between Boiling Water Reactors (BWR) and Pressurized Water Reactors (PWR) Nuclear power reactors (5 Marks)

QUESTION 4(25 MARKS)

- (a) Kenya intends to meet part of its projected energy requirements in the vision 2030 from nuclear energy. Discuss the advantages and disadvantages of nuclear energy and country's preparedness for investment in nuclear power. (6 marks)
- (b) Steam at 20 bar and 300°C is supplied to a turbine in a cycle and is bled at 5bar. The bled-steam just comes out dry saturated. This steam heats water in an open feed heater to its saturation state. The rest of the steam in the turbine expands to a condenser pressure of 0.1 bar. Assuming the turbine efficiency to be the same before and after bleeding, find:
- (i) The turbine efficiency and the steam quality at the exit of the last stage;
 - (ii) The quantity of bled steam per kg of steam flow at the turbine inlet;
 - (iii) Power output per (kg/s) of steam flow, neglect the feed pump work. (9 Marks)
- (c) A combined power plant consists of a gas turbine unit and a steam turbine unit. The exhaust gas from the open cycle gas turbine is the supply gas to the steam generator of the steam turbine cycle at which additional fuel is burned in the gas. Draw a line diagram of the unit.
- The pressure ratio for the gas turbine unit is 7.5 to 1, the air inlet temperature is 15°C and the maximum cycle temperature is 750°C . Combustion in the steam generator raises the gas temperature to 750°C and the gas leaves the generator to atmosphere at 100°C . The steam is supplied to the turbine at 50 bar and 600°C and the condenser pressure is 0.1 bar.
- Calculate the flow rates of air and steam required for a total power output of 200MW, the power output of each turbine and the thermal efficiency of the plant. Assume ideal cycle for the two units. What would be the overall air/ fuel ratio?

Show also the line diagram for the combined Power plant and the T-S diagram for the ideal gas turbine and Ideal Steam turbine cycles.

For the combustion gases take $c_p = 1.11 \text{ kJ/kg K}$ and $\gamma = 1.33$ and neglect the effect of the mass flow rate of the fuel on that of the air. Take Calorific value of fuel as 43000 kJ/kg . (10 Marks)

QUESTION 5 (25 MARKS)

(a) Explain using schematic diagrams the following types of geothermal power plants

- (i) Dry steam power plant
- (ii) Single flash steam power plant
- (iii) Binary cycle power plant
- (iv) Double flash steam power plant (8 Marks)

(b) Outline the advantages and disadvantages of diesel power plants (7 marks)

(c) An ideal dual combustion cycle has a volume ratio of the adiabatic compression of 16:1. At the beginning of the adiabatic compression, the pressure, volume and temperature of the gas are 100 kN/m^2 , 0.084 m^3 and 28°C respectively. The maximum pressure and temperature of the cycle are 5 MN/m^2 and 1300°C , respectively.

For the cycle determine:

- (i) The pressure, volume and temperature at the cycle process change points
- (ii) The net work done
- (iii) The thermal efficiency
- (iv) The heat received
- (v) The work ratio
- (vi) The mean effective pressure
- (vii) The carnot efficiency within the cycle temperature limits (10 Marks)

Take $C_p = 1.005 \text{ kJ/kgK}$ and $C_v = 0.717 \text{ kJ/gK}$

Saturated Water and Steam

T [°C]	p_s [bar]	v_g [m ³ /kg]	h_f [kJ/kg]	h_g [kJ/kg]	s_f [kJ/kg K]	s_{fg} [kJ/kg K]	s_g [kJ/kg K]
0.01	0.006112	206.1	0*	2500.8	2500.8	0†	9.155
1	0.006566	192.6	4.2	2498.3	2502.5	0.015	9.113
2	0.007054	179.9	8.4	2495.9	2504.3	0.031	9.071
3	0.007575	168.2	12.6	2493.6	2506.2	0.046	9.030
4	0.008129	157.3	16.8	2491.3	2508.1	0.061	8.989
5	0.008719	147.1	21.0	2488.9	2509.9	0.076	8.948
6	0.009346	137.8	25.2	2486.6	2511.8	0.091	8.908
7	0.01001	129.1	29.4	2484.3	2513.7	0.106	8.868
8	0.01072	121.0	33.6	2481.9	2515.5	0.121	8.828
9	0.01147	113.4	37.8	2479.6	2517.4	0.136	8.788
10	0.01227	106.4	42.0	2477.2	2519.2	0.151	8.749
11	0.01312	99.90	46.2	2474.9	2521.1	0.166	8.710
12	0.01401	93.83	50.4	2472.5	2522.9	0.180	8.671
13	0.01497	88.17	54.6	2470.2	2524.8	0.195	8.633
14	0.01597	82.89	58.8	2467.8	2526.6	0.210	8.594
15	0.01704	77.97	62.9	2465.5	2528.4	0.224	8.556
16	0.01817	73.38	67.1	2463.1	2530.2	0.239	8.518
17	0.01936	69.09	71.3	2460.8	2532.1	0.253	8.481
18	0.02063	65.08	75.5	2458.4	2533.9	0.268	8.444
19	0.02196	61.34	79.7	2456.0	2535.7	0.282	8.407
20	0.02337	57.84	83.9	2453.7	2537.6	0.296	8.370
21	0.02486	54.56	88.0	2451.4	2539.4	0.310	8.334
22	0.02642	51.49	92.2	2449.0	2541.2	0.325	8.297
23	0.02808	48.62	96.4	2446.6	2543.0	0.339	8.261
24	0.02982	45.92	100.6	2444.2	2544.8	0.353	8.226
25	0.03166	43.40	104.8	2441.8	2546.6	0.367	8.190
26	0.03360	41.03	108.9	2439.5	2548.4	0.381	8.155
27	0.03564	38.81	113.1	2437.2	2550.3	0.395	8.120
28	0.03778	36.73	117.3	2434.8	2552.1	0.409	8.085
29	0.04004	34.77	121.5	2432.4	2553.9	0.423	8.050
30	0.04242	32.93	125.7	2430.0	2555.7	0.436	8.016
32	0.04754	29.57	134.0	2425.3	2559.3	0.464	7.948
34	0.05318	26.60	142.4	2420.5	2562.9	0.491	7.881
36	0.05940	23.97	150.7	2415.8	2566.5	0.518	7.814
38	0.06624	21.63	159.1	2411.0	2570.1	0.545	7.749
40	0.07375	19.55	167.5	2406.2	2573.7	0.572	7.684
42	0.08198	17.69	175.8	2401.4	2577.2	0.599	7.620
44	0.09100	16.03	184.2	2396.6	2580.8	0.625	7.557
46	0.1009	14.56	192.5	2391.8	2584.3	0.651	7.494
48	0.1116	13.23	200.9	2387.0	2587.9	0.678	7.433
50	0.1233	12.04	209.3	2382.1	2591.4	0.704	7.371
55	0.1574	9.578	230.2	2370.1	2600.3	0.768	7.223
60	0.1992	7.678	251.1	2357.9	2609.0	0.831	7.078
65	0.2501	6.201	272.0	2345.7	2617.7	0.893	6.937
70	0.3116	5.045	293.0	2333.3	2626.3	0.955	6.800
75	0.3855	4.133	313.9	2320.8	2634.7	1.015	6.666
80	0.4736	3.408	334.9	2308.3	2643.2	1.075	6.536
85	0.5780	2.828	355.9	2295.6	2651.5	1.134	6.410
90	0.7011	2.361	376.9	2282.8	2659.7	1.192	6.286
95	0.8453	1.982	398.0	2269.8	2667.8	1.250	6.166
100	1.01325	1.673	419.1	2256.7	2675.8	1.307	6.048

† u and s are chosen to be zero for saturated liquid at the triple point.

Note: values of v_f can be found on p. 10.

p [bar]	T_s [°C]	v_g [m³/kg]	u_f [kJ/kg]	u_g [kJ/kg]	h_f [kJ/kg]	h_{fg} [kJ/kg]	h_g [kJ/kg]	s_f [kJ/kg K]	s_{fg} [kJ/kg K]	s_g [kJ/kg K]
0.006112	0.01	206.1	0†	2375	0*	2501	2501	0†	9.155	9.155
0.010	7.0	129.2	29	2385	29	2485	2514	0.106	8.868	8.974
0.015	13.0	87.98	55	2393	55	2470	2525	0.196	8.631	8.827
0.020	17.5	67.01	73	2399	73	2460	2533	0.261	8.462	8.723
0.025	21.1	54.26	88	2403	88	2451	2539	0.312	8.330	8.642
0.030	24.1	45.67	101	2408	101	2444	2545	0.354	8.222	8.576
0.035	26.7	39.48	112	2412	112	2438	2550	0.391	8.130	8.521
0.040	29.0	34.80	121	2415	121	2433	2554	0.422	8.051	8.473
0.045	31.0	31.14	130	2418	130	2428	2558	0.451	7.980	8.431
0.050	32.9	28.20	138	2420	138	2423	2561	0.476	7.918	8.394
0.055	34.6	25.77	145	2422	145	2419	2564	0.500	7.860	8.360
0.060	36.2	23.74	152	2425	152	2415	2567	0.521	7.808	8.329
0.065	37.7	22.02	158	2427	158	2412	2570	0.541	7.760	8.301
0.070	39.0	20.53	163	2428	163	2409	2572	0.559	7.715	8.274
0.075	40.3	19.24	169	2430	169	2405	2574	0.576	7.674	8.250
0.080	41.5	18.10	174	2432	174	2402	2576	0.593	7.634	8.227
0.085	42.7	17.10	179	2434	179	2400	2579	0.608	7.598	8.206
0.090	43.8	16.20	183	2435	183	2397	2580	0.622	7.564	8.186
0.095	44.8	15.40	188	2436	188	2394	2582	0.636	7.531	8.167
0.100	45.8	14.67	192	2437	192	2392	2584	0.649	7.500	8.149
0.12	49.4	12.36	207	2442	207	2383	2590	0.696	7.389	8.085
0.14	52.6	10.69	220	2446	220	2376	2596	0.737	7.294	8.031
0.16	55.3	9.432	232	2450	232	2369	2601	0.772	7.213	7.985
0.18	57.8	8.444	242	2453	242	2363	2605	0.804	7.140	7.944
0.20	60.1	7.648	251	2456	251	2358	2609	0.832	7.075	7.907
0.22	62.2	6.994	260	2459	260	2353	2613	0.858	7.016	7.874
0.24	64.1	6.445	268	2461	268	2348	2616	0.882	6.962	7.844
0.26	65.9	5.979	276	2464	276	2343	2619	0.904	6.913	7.817
0.28	67.5	5.578	283	2466	283	2339	2622	0.925	6.866	7.791
0.30	69.1	5.228	289	2468	289	2336	2625	0.944	6.823	7.767
0.32	70.6	4.921	295	2470	295	2332	2627	0.962	6.783	7.745
0.34	72.0	4.649	302	2472	302	2328	2630	0.980	6.745	7.725
0.36	73.4	4.407	307	2473	307	2325	2632	0.996	6.709	7.705
0.38	74.7	4.189	312	2475	312	2322	2634	1.011	6.675	7.686
0.40	75.9	3.992	318	2476	318	2318	2636	1.026	6.643	7.669
0.42	77.1	3.814	323	2478	323	2315	2638	1.040	6.612	7.652
0.44	78.2	3.651	327	2479	327	2313	2640	1.054	6.582	7.636
0.46	79.3	3.502	332	2481	332	2310	2642	1.067	6.554	7.621
0.48	80.3	3.366	336	2482	336	2308	2644	1.079	6.528	7.607
0.50	81.3	3.239	340	2483	340	2305	2645	1.091	6.502	7.593
0.55	83.7	2.964	351	2486	351	2298	2649	1.119	6.442	7.561
0.60	86.0	2.731	360	2489	360	2293	2653	1.145	6.386	7.531
0.65	88.0	2.535	369	2492	369	2288	2657	1.169	6.335	7.504
0.70	90.0	2.364	377	2494	377	2283	2660	1.192	6.286	7.478
0.75	91.8	2.217	384	2496	384	2278	2662	1.213	6.243	7.456
0.80	93.5	2.087	392	2498	392	2273	2665	1.233	6.201	7.434
0.85	95.2	1.972	399	2500	399	2269	2668	1.252	6.162	7.414
0.90	96.7	1.869	405	2502	405	2266	2671	1.270	6.124	7.394
0.95	98.2	1.777	411	2504	411	2262	2673	1.287	6.089	7.376
1.00	99.6	1.694	417	2506	417	2258	2675	1.303	6.056	7.359

$$\begin{aligned}
 * \quad \frac{h_f}{[\text{kJ/kg}]} &= \frac{p v_f}{[\text{kJ/kg}]} = \frac{p}{[\text{bar}]} \times \frac{10^5 [\text{N}]}{[\text{m}^2]} \times \frac{v_f}{[\text{m}^3/\text{kg}]} \times \left[\frac{\text{m}^3}{\text{kg}} \right] \times \frac{[\text{kJ}]}{10^3 [\text{N m}]} \times \frac{1}{[\text{kJ/kg}]} \\
 &= \frac{p}{[\text{bar}]} \times \frac{v_f}{[\text{m}^3/\text{kg}]} \times 10^2 = 0.006112 \times 0.0010002 \times 10^2 = 0.0006112
 \end{aligned}$$

Saturated Water and Steam

p [bar]	T_s [°C]	v_g [m ³ /kg]	u_f [kJ/kg]	u_g [kJ/kg]	h_f [kJ/kg]	h_{fg} [kJ/kg]	h_g [kJ/kg]	s_f [kJ/kg K]	s_{fg} [kJ/kg K]	s_g [kJ/kg K]
1.0	99.6	1.694	417	2506	417	2258	2675	1.303	6.056	7.359
1.1	102.3	1.549	429	2510	429	2251	2680	1.333	5.994	7.327
1.2	104.8	1.428	439	2512	439	2244	2683	1.361	5.937	7.298
1.3	107.1	1.325	449	2515	449	2238	2687	1.387	5.884	7.271
1.4	109.3	1.236	458	2517	458	2232	2690	1.411	5.835	7.246
1.5	111.4	1.159	467	2519	467	2226	2693	1.434	5.789	7.223
1.6	113.3	1.091	475	2521	475	2221	2696	1.455	5.747	7.202
1.7	115.2	1.031	483	2524	483	2216	2699	1.475	5.707	7.182
1.8	116.9	0.9774	491	2526	491	2211	2702	1.494	5.669	7.163
1.9	118.6	0.9292	498	2528	498	2206	2704	1.513	5.632	7.145
2.0	120.2	0.8856	505	2530	505	2202	2707	1.530	5.597	7.127
2.1	121.8	0.8461	511	2531	511	2198	2709	1.547	5.564	7.111
2.2	123.3	0.8100	518	2533	518	2193	2711	1.563	5.533	7.096
2.3	124.7	0.7770	524	2534	524	2189	2713	1.578	5.503	7.081
2.4	126.1	0.7466	530	2536	530	2185	2715	1.593	5.474	7.067
2.5	127.4	0.7186	535	2537	535	2182	2717	1.607	5.446	7.053
2.6	128.7	0.6927	541	2539	541	2178	2719	1.621	5.419	7.040
2.7	130.0	0.6686	546	2540	546	2174	2720	1.634	5.393	7.027
2.8	131.2	0.6462	551	2541	551	2171	2722	1.647	5.368	7.015
2.9	132.4	0.6253	556	2543	556	2168	2724	1.660	5.344	7.004
3.0	133.5	0.6057	561	2544	561	2164	2725	1.672	5.321	6.993
3.5	138.9	0.5241	584	2549	584	2148	2732	1.727	5.214	6.941
4.0	143.6	0.4623	605	2554	605	2134	2739	1.776	5.121	6.897
4.5	147.9	0.4139	623	2558	623	2121	2744	1.820	5.037	6.857
5.0	151.8	0.3748	639	2562	640	2109	2749	1.860	4.962	6.822
5.5	155.5	0.3427	655	2565	656	2097	2753	1.897	4.893	6.790
6	158.8	0.3156	669	2568	670	2087	2757	1.931	4.830	6.761
7	165.0	0.2728	696	2573	697	2067	2764	1.992	4.717	6.709
8	170.4	0.2403	720	2577	721	2048	2769	2.046	4.617	6.663
9	175.4	0.2149	742	2581	743	2031	2774	2.094	4.529	6.623
10	179.9	0.1944	762	2584	763	2015	2778	2.138	4.448	6.586
11	184.1	0.1774	780	2586	781	2000	2781	2.179	4.375	6.554
12	188.0	0.1632	797	2588	798	1986	2784	2.216	4.307	6.523
13	191.6	0.1512	813	2590	815	1972	2787	2.251	4.244	6.495
14	195.0	0.1408	828	2593	830	1960	2790	2.284	4.185	6.469
15	198.3	0.1317	843	2595	845	1947	2792	2.315	4.130	6.445
16	201.4	0.1237	857	2596	859	1935	2794	2.344	4.078	6.422
17	204.3	0.1167	870	2597	872	1923	2795	2.372	4.028	6.400
18	207.1	0.1104	883	2598	885	1912	2797	2.398	3.981	6.379
19	209.8	0.1047	895	2599	897	1901	2798	2.423	3.936	6.359
20	212.4	0.09957	907	2600	909	1890	2799	2.447	3.893	6.340
22	217.2	0.09069	928	2601	931	1870	2801	2.492	3.813	6.305
24	221.8	0.08323	949	2602	952	1850	2802	2.534	3.738	6.272
26	226.0	0.07689	969	2603	972	1831	2803	2.574	3.668	6.242
28	230.0	0.07142	988	2603	991	1812	2803	2.611	3.602	6.213
30	233.8	0.06665	1004	2603	1008	1795	2803	2.645	3.541	6.186
32	237.4	0.06246	1021	2603	1025	1778	2803	2.679	3.482	6.161
34	240.9	0.05875	1038	2603	1042	1761	2803	2.710	3.426	6.136
36	244.2	0.05544	1054	2602	1058	1744	2802	2.740	3.373	6.113
38	247.3	0.05246	1068	2602	1073	1729	2802	2.769	3.322	6.091
40	250.3	0.04977	1082	2602	1087	1714	2801	2.797	3.273	6.070

Saturated Water and Steam

p [bar]	T_s [°C]	v_g [m ³ /kg]	u_f [kJ/kg]	u_g [kJ/kg]	h_f [kJ/kg]	h_{fg} [kJ/kg]	h_g [kJ/kg]	s_f [kJ/kg K]	s_{fg} [kJ/kg K]	s_g [kJ/kg K]
40	250.3	0.04977	1082	2602	1087	1714	2801	2.797	3.273	6.070
42	253.2	0.04732	1097	2601	1102	1698	2800	2.823	3.226	6.049
44	256.0	0.04509	1109	2600	1115	1683	2798	2.849	3.180	6.029
46	258.8	0.04305	1123	2599	1129	1668	2797	2.874	3.136	6.010
48	261.4	0.04117	1136	2598	1142	1654	2796	2.897	3.094	5.991
50	263.9	0.03944	1149	2597	1155	1639	2794	2.921	3.052	5.973
55	269.9	0.03563	1178	2594	1185	1605	2790	2.976	2.955	5.931
60	275.6	0.03244	1206	2590	1214	1570	2784	3.027	2.863	5.890
65	280.8	0.02972	1232	2586	1241	1538	2779	3.076	2.775	5.851
70	285.8	0.02737	1258	2581	1267	1505	2772	3.122	2.692	5.814
75	290.5	0.02532	1283	2576	1293	1473	2766	3.166	2.613	5.779
80	295.0	0.02352	1306	2570	1317	1441	2758	3.207	2.537	5.744
85	299.2	0.02192	1329	2565	1341	1410	2751	3.248	2.463	5.711
90	303.3	0.02048	1351	2559	1364	1379	2743	3.286	2.393	5.679
95	307.2	0.01919	1372	2552	1386	1348	2734	3.324	2.323	5.647
100	311.0	0.01802	1393	2545	1408	1317	2725	3.360	2.255	5.615
105	314.6	0.01696	1414	2537	1429	1286	2715	3.395	2.189	5.584
110	318.0	0.01598	1434	2529	1450	1255	2705	3.430	2.123	5.553
115	321.4	0.01508	1454	2522	1471	1224	2695	3.463	2.060	5.523
120	324.6	0.01426	1473	2514	1491	1194	2685	3.496	1.997	5.493
125	327.8	0.01349	1492	2505	1511	1163	2674	3.529	1.934	5.463
130	330.8	0.01278	1511	2496	1531	1131	2662	3.561	1.872	5.433
135	333.8	0.01211	1530	2487	1551	1099	2650	3.592	1.811	5.403
140	336.6	0.01149	1548	2477	1571	1067	2638	3.623	1.750	5.373
145	339.4	0.01090	1567	2467	1591	1034	2625	3.654	1.689	5.343
150	342.1	0.01035	1585	2456	1610	1001	2611	3.685	1.627	5.312
155	344.8	0.00982	1604	2445	1630	967	2597	3.715	1.565	5.280
160	347.3	0.00932	1623	2433	1650	932	2582	3.746	1.502	5.248
165	349.8	0.00884	1641	2420	1670	895	2565	3.777	1.437	5.214
170	352.3	0.00838	1660	2406	1690	858	2548	3.808	1.373	5.181
175	354.6	0.00794	1679	2391	1711	819	2530	3.839	1.305	5.144
180	357.0	0.00751	1699	2375	1732	778	2510	3.872	1.236	5.108
185	359.2	0.00709	1719	2358	1754	735	2489	3.905	1.163	5.068
190	361.4	0.00668	1740	2339	1777	689	2466	3.941	1.086	5.027
195	363.6	0.00627	1762	2318	1801	639	2440	3.977	1.004	4.981
200	365.7	0.00585	1786	2294	1827	584	2411	4.014	0.914	4.928
202	366.5	0.00569	1796	2283	1838	560	2398	4.031	0.875	4.906
204	367.4	0.00552	1806	2271	1849	535	2384	4.049	0.835	4.884
206	368.2	0.00534	1817	2259	1861	508	2369	4.067	0.792	4.859
208	369.0	0.00517	1829	2245	1874	479	2353	4.087	0.745	4.832
210	369.8	0.00498	1842	2231	1889	447	2336	4.108	0.695	4.803
212	370.6	0.00479	1856	2214	1904	412	2316	4.131	0.640	4.771
214	371.4	0.00458	1871	2196	1921	373	2294	4.157	0.579	4.736
216	372.1	0.00436	1888	2174	1940	328	2268	4.186	0.508	4.694
218	372.9	0.00409	1911	2146	1965	270	2235	4.224	0.417	4.641
220	373.7	0.00368	1949	2097	2008	170	2178	4.289	0.263	4.552
221.2	374.15	0.00317	2014	2014	2084	0	2084	4.406	0.000	4.406

Superheated Steam†

$p/[\text{bar}]$ ($T_s/[^{\circ}\text{C}]$)		T [$^{\circ}\text{C}$]	50	100	150	200	250	300	400	500
0	$u = h - RT$ at $p = 0$	v								
		u	2446	2517	2589	2662	2737	2812	2969	3132
		h	2595	2689	2784	2880	2978	3077	3280	3489
		s								
0.006112 (0.01)	v_g 206.1	v	243.9	281.7	319.5	357.3	395.0	432.8	508.3	583.8
	u_g 2375	u	2446	2517	2589	2662	2737	2812	2969	3132
	h_g 2501	h	2595	2689	2784	2880	2978	3077	3280	3489
	s_g 9.155	s	9.468	9.739	9.978	10.193	10.390	10.571	10.897	11.187
0.01 (7.0)	v_g 129.2	v	149.1	172.2	195.3	218.4	241.4	264.5	310.7	356.8
	u_g 2385	u	2446	2517	2589	2662	2737	2812	2969	3132
	h_g 2514	h	2595	2689	2784	2880	2978	3077	3280	3489
	s_g 8.974	s	9.241	9.512	9.751	9.966	10.163	10.344	10.670	10.960
0.05 (32.9)	v_g 28.20	v	29.78	34.42	39.04	43.66	48.28	52.90	62.13	71.36
	u_g 2420	u	2445	2516	2589	2662	2737	2812	2969	3132
	h_g 2561	h	2594	2688	2784	2880	2978	3077	3280	3489
	s_g 8.394	s	8.496	8.768	9.008	9.223	9.420	9.601	9.927	10.217
0.1 (45.8)	v_g 14.67	v	14.87	17.20	19.51	21.83	24.14	26.45	31.06	35.68
	u_g 2437	u	2443	2516	2588	2662	2736	2812	2969	3132
	h_g 2584	h	2592	2688	2783	2880	2977	3077	3280	3489
	s_g 8.149	s	8.173	8.447	8.688	8.903	9.100	9.281	9.607	9.897
0.5 (81.3)	v_g 3.239	v		3.420	3.890	4.356	4.821	5.284	6.209	7.134
	u_g 2483	u		2512	2585	2660	2735	2812	2969	3132
	h_g 2645	h		2683	2780	2878	2976	3076	3279	3489
	s_g 7.593	s		7.694	7.940	8.158	8.355	8.537	8.864	9.154
0.75 (91.8)	v_g 2.217	v		2.271	2.588	2.901	3.211	3.521	4.138	4.755
	u_g 2496	u		2510	2585	2659	2734	2811	2969	3132
	h_g 2662	h		2680	2779	2877	2975	3075	3279	3489
	s_g 7.456	s		7.500	7.750	7.969	8.167	8.349	8.676	8.967
1 (99.6)	v_g 1.694	v		1.696	1.937	2.173	2.406	2.639	3.103	3.565
	u_g 2506	u		2506	2583	2659	2734	2811	2968	3131
	h_g 2675	h		2676	2777	2876	2975	3075	3278	3488
	s_g 7.359	s		7.360	7.614	7.834	8.033	8.215	8.543	8.834
1.01325 (100.0)	v_g 1.673	v			1.912	2.145	2.375	2.604	3.062	3.519
	u_g 2506	u			2583	2659	2734	2811	2968	3131
	h_g 2676	h			2777	2876	2975	3075	3278	3488
	s_g 7.355	s			7.608	7.828	8.027	8.209	8.537	8.828
1.5 (111.4)	v_g 1.159	v			1.286	1.445	1.601	1.757	2.067	2.376
	u_g 2519	u			2580	2656	2733	2809	2967	3131
	h_g 2693	h			2773	2873	2973	3073	3277	3488
	s_g 7.223	s			7.420	7.643	7.843	8.027	8.355	8.646
2 (120.2)	v_g 0.8856	v			0.9602	1.081	1.199	1.316	1.549	1.781
	u_g 2530	u			2578	2655	2731	2809	2967	3131
	h_g 2707	h			2770	2871	2971	3072	3277	3487
	s_g 7.127	s			7.280	7.507	7.708	7.892	8.221	8.513
3 (133.5)	v_g 0.6057	v			0.6342	0.7166	0.7965	0.8754	1.031	1.187
	u_g 2544	u			2572	2651	2729	2807	2966	3130
	h_g 2725	h			2762	2866	2968	3070	3275	3486
	s_g 6.993	s			7.078	7.312	7.517	7.702	8.032	8.324
4 (143.6)	v_g 0.4623	$v/[\text{m}^3/\text{kg}]$			0.4710	0.5345	0.5953	0.6549	0.7725	0.8893
	u_g 2554	$u/[\text{kJ}/\text{kg}]$			2565	2648	2727	2805	2965	3129
	h_g 2739	$h/[\text{kJ}/\text{kg}]$			2753	2862	2965	3067	3274	3485
	s_g 6.897	$s/[\text{kJ}/\text{kg K}]$			6.929	7.172	7.379	7.566	7.898	8.191

† The entries in all tables are regarded as pure numbers and therefore the symbols for the physical quantities should be divided by the appropriate units as shown for the entries at $p/[\text{bar}] = 4$. Because of lack of space, this has not been done consistently in the superheat and supercritical tables on pp. 6–9 and in the tables on pp. 11 and 23.

Superheated Steam*

$p/[\text{bar}]$ $(T_s/[^{\circ}\text{C}])$		T $[^{\circ}\text{C}]$	200	250	300	350	400	450	500	600
5 (151.8)	v_g	0.3748	v	0.4252	0.4745	0.5226	0.5701	0.6172	0.6641	0.8040
	u_g	2562	u	2644	2725	2804	2883	2963	3045	3300
	h_g	2749	h	2857	2962	3065	3168	3272	3377	3702
	s_g	6.822	s	7.060	7.271	7.460	7.633	7.793	7.944	8.351
6 (158.8)	v_g	0.3156	v	0.3522	0.3940	0.4344	0.4743	0.5136	0.5528	0.6697
	u_g	2568	u	2640	2722	2801	2881	2962	3044	3299
	h_g	2757	h	2851	2958	3062	3166	3270	3376	3701
	s_g	6.761	s	6.968	7.182	7.373	7.546	7.707	7.858	8.267
7 (165.0)	v_g	0.2728	v	0.3001	0.3364	0.3714	0.4058	0.4397	0.4734	0.5737
	u_g	2573	u	2636	2720	2800	2880	2961	3043	3298
	h_g	2764	h	2846	2955	3060	3164	3269	3374	3700
	s_g	6.709	s	6.888	7.106	7.298	7.473	7.634	7.786	8.195
8 (170.4)	v_g	0.2403	v	0.2610	0.2933	0.3242	0.3544	0.3842	0.4138	0.5018
	u_g	2577	u	2631	2716	2798	2878	2960	3042	3298
	h_g	2769	h	2840	2951	3057	3162	3267	3373	3699
	s_g	6.663	s	6.817	7.040	7.233	7.409	7.571	7.723	8.132
9 (175.4)	v_g	0.2149	v	0.2305	0.2597	0.2874	0.3144	0.3410	0.3674	0.4458
	u_g	2581	u	2628	2714	2796	2877	2959	3041	3298
	h_g	2774	h	2835	2948	3055	3160	3266	3372	3699
	s_g	6.623	s	6.753	6.980	7.176	7.352	7.515	7.667	8.077
10 (179.9)	v_g	0.1944	v	0.2061	0.2328	0.2580	0.2825	0.3065	0.3303	0.4010
	u_g	2584	u	2623	2711	2794	2875	2957	3040	3297
	h_g	2778	h	2829	2944	3052	3158	3264	3370	3698
	s_g	6.586	s	6.695	6.926	7.124	7.301	7.464	7.617	8.028
15 (198.3)	v_g	0.1317	v	0.1324	0.1520	0.1697	0.1865	0.2029	0.2191	0.2667
	u_g	2595	u	2597	2697	2784	2868	2952	3035	3294
	h_g	2792	h	2796	2925	3039	3148	3256	3364	3694
	s_g	6.445	s	6.452	6.711	6.919	7.102	7.268	7.423	7.838
20 (212.4)	v_g	0.0996	v		0.1115	0.1255	0.1386	0.1511	0.1634	0.1995
	u_g	2600	u		2681	2774	2861	2946	3030	3291
	h_g	2799	h		2904	3025	3138	3248	3357	3690
	s_g	6.340	s		6.547	6.768	6.957	7.126	7.283	7.701
30 (233.8)	v_g	0.0666	v		0.0706	0.0812	0.0905	0.0993	0.1078	0.1324
	u_g	2603	u		2646	2751	2845	2933	3020	3285
	h_g	2803	h		2858	2995	3117	3231	3343	3682
	s_g	6.186	s		6.289	6.541	6.744	6.921	7.082	7.507
40 (250.3)	v_g	0.0498	v			0.0588	0.0664	0.0733	0.0800	0.0988
	u_g	2602	u			2728	2828	2921	3010	3279
	h_g	2801	h			2963	3094	3214	3330	3674
	s_g	6.070	s			6.364	6.584	6.769	6.935	7.368
50 (263.9)	v_g	0.0394	v			0.0453	0.0519	0.0578	0.0632	0.0786
	u_g	2597	u			2700	2810	2907	3000	3273
	h_g	2794	h			2927	3070	3196	3316	3666
	s_g	5.973	s			6.212	6.451	6.646	6.818	7.258
60 (275.6)	v_g	0.0324	v			0.0362	0.0422	0.0473	0.0521	0.0652
	u_g	2590	u			2670	2792	2893	2988	3266
	h_g	2784	h			2887	3045	3177	3301	3657
	s_g	5.890	s			6.071	6.336	6.541	6.719	7.166
70 (285.8)	v_g	0.0274	$v/[\text{m}^3/\text{kg}]$			0.0295	0.0352	0.0399	0.0441	0.0556
	u_g	2581	$u/[\text{kJ}/\text{kg}]$			2634	2772	2879	2978	3260
	h_g	2772	$h/[\text{kJ}/\text{kg}]$			2841	3018	3158	3287	3649
	s_g	5.814	$s/[\text{kJ}/\text{kg K}]$			5.934	6.231	6.448	6.632	7.088

* See footnote on p. 6.

Superheated Steam*

$p/[\text{bar}]$ ($T_s/[^{\circ}\text{C}]$)			T [$^{\circ}\text{C}$]	350	375	400	425	450	500	600	700
80 (295.0)	v	0.02352	$v/10^{-2}$	2.994	3.220	3.428	3.625	3.812	4.170	4.839	5.476
	h	2758	h	2990	3067	3139	3207	3272	3398	3641	3881
	s	5.744	s	6.133	6.255	6.364	6.463	6.555	6.723	7.019	7.279
90 (303.3)	v	0.02048	$v/10^{-2}$	2.578	2.794	2.991	3.173	3.346	3.673	4.279	4.852
	h	2743	h	2959	3042	3118	3189	3256	3385	3633	3874
	s_g	5.679	s	6.039	6.171	6.286	6.390	6.484	6.657	6.958	7.220
100 (311.0)	v	0.01802	$v/10^{-2}$	2.241	2.453	2.639	2.812	2.972	3.275	3.831	4.353
	h	2725	h	2926	3017	3097	3172	3241	3373	3624	3868
	s	5.615	s	5.947	6.091	6.213	6.321	6.419	6.596	6.902	7.166
110 (318.0)	v	0.01598	$v/10^{-2}$	1.960	2.169	2.350	2.514	2.666	2.949	3.465	3.945
	h	2705	h	2889	2989	3075	3153	3225	3360	3616	3862
	s_g	5.553	s	5.856	6.014	6.143	6.257	6.358	6.539	6.850	7.117
120 (324.6)	v	0.01426	$v/10^{-2}$	1.719	1.931	2.107	2.265	2.410	2.677	3.159	3.605
	h	2685	h	2849	2960	3052	3134	3209	3348	3607	3856
	s_g	5.493	s	5.762	5.937	6.076	6.195	6.301	6.487	6.802	7.072
130 (330.8)	v_g	0.01278	$v/10^{-2}$	1.509	1.726	1.901	2.053	2.193	2.447	2.901	3.318
	h	2662	h	2804	2929	3028	3114	3192	3335	3599	3850
	s	5.433	s	5.664	5.862	6.011	6.136	6.246	6.437	6.758	7.030
140 (336.6)	v	0.01149	$v/10^{-2}$	1.321	1.548	1.722	1.872	2.006	2.250	2.679	3.071
	h_g	2638	h	2753	2896	3003	3093	3175	3322	3590	3843
	s_g	5.373	s	5.559	5.784	5.946	6.079	6.193	6.390	6.716	6.991
150 (342.1)	v	0.01035	$v/10^{-2}$	1.146	1.391	1.566	1.714	1.844	2.078	2.487	2.857
	h	2611	h	2693	2861	2977	3073	3157	3309	3581	3837
	s_g	5.312	s	5.443	5.707	5.883	6.023	6.142	6.345	6.677	6.954
160 (347.3)	v_g	0.00932	$v/10^{-2}$	0.976	1.248	1.427	1.573	1.702	1.928	2.319	2.670
	h	2582	h	2617	2821	2949	3051	3139	3295	3573	3831
	s_g	5.248	s	5.304	5.626	5.820	5.968	6.093	6.301	6.639	6.919
170 (352.3)	v	0.00838	$v/10^{-2}$		1.117	1.303	1.449	1.576	1.796	2.171	2.506
	h	2548	h		2778	2920	3028	3121	3281	3564	3825
	s_g	5.181	s		5.541	5.756	5.914	6.044	6.260	6.603	6.886
180 (357.0)	v_g	0.00751	$v/10^{-2}$		0.997	1.191	1.338	1.463	1.678	2.039	2.359
	h	2510	h		2729	2888	3004	3102	3268	3555	3818
	s_g	5.108	s		5.449	5.691	5.861	5.997	6.219	6.569	6.855
190 (361.4)	v	0.00668	$v/10^{-2}$		0.882	1.089	1.238	1.362	1.572	1.921	2.228
	h	2466	h		2674	2855	2980	3082	3254	3546	3812
	s_g	5.027	s		5.348	5.625	5.807	5.950	6.180	6.536	6.825
200 (365.7)	v	0.00585	$v/10^{-2}[\text{m}^3/\text{kg}]$		0.768	0.995	1.147	1.270	1.477	1.815	2.110
	h	2411	$h/[\text{kJ}/\text{kg}]$		2605	2819	2955	3062	3239	3537	3806
	s_g	4.928	$s/[\text{kJ}/\text{kg K}]$		5.228	5.556	5.753	5.904	6.142	6.505	6.796
210 (369.8)	v	0.00498	$v/10^{-2}$		0.650	0.908	1.064	1.187	1.390	1.719	2.003
	h	2336	h		2500	2781	2928	3041	3225	3528	3799
	s_g	4.803	s		5.050	5.484	5.699	5.859	6.105	6.474	6.768
220 (373.7)	v	0.00368	$v/10^{-2}$		0.450	0.825	0.987	1.111	1.312	1.632	1.906
	h	2178	h		2300	2738	2900	3020	3210	3519	3793
	s_g	4.552	s		4.725	5.409	5.645	5.813	6.068	6.444	6.742
221.2 (374.15)	v_c	0.00317	$v/10^{-2}$	0.163	0.351	0.816	0.978	1.103	1.303	1.622	1.895
	h_c	2084	h	1637	2139	2733	2896	3017	3208	3518	3792
	s_c	4.406	s	3.708	4.490	5.398	5.638	5.807	6.064	6.441	6.739

* See footnote on p. 6.

Note: linear interpolation is not accurate near the critical point.